

**Amendments to the Specification:**

*On page 1, after the title, insert the following:*

**CROSS-REFERENCE TO RELATED APPLICATION**

This application is the U.S. national phase of PCT Appln. No. PCT/EP2005/002887 filed March 17, 2005, which claims priority to German application 10 2004 014 704.3 filed March 25, 2004.

**BACKGROUND OF THE INVENTION**

1. Field of the Invention

*On page 1, before the paragraph beginning on line 7, please add the following:*

2. Description of the Related Art

*Please amend the paragraph beginning on page 1, line 36 as shown below:*

In 1907, Pickering described for the first time the preparation of emulsions which were stabilized only by addition of various solids, such as basic copper sulfates, basic iron sulfates or other metal salts. This type of emulsion is also referred to as a "Pickering emulsion[[s]]". Basic investigations showed that a characteristic of Pickering emulsions is that solid particles are arranged at the interface between the two liquid phases and form a barrier there to the coalescence of the disperse phase.

*On page 2, before line 15, please insert the following heading:*

**SUMMARY OF THE INVENTION**

*Please amend the paragraph beginning on page 2, line 15 as shown below:*

It was an object of the invention to overcome the disadvantages of the prior art, in particular to provide low-viscosity and sedimentation-stable emulsions having a dispersed phase with a small particle diameter of the disperse phase. These and other objects are achieved by employing as a dispersion stabilizer a pyrogenic silica which has been partially silylated, and has specific surface properties.

*Please amend the paragraph beginning on page 2, line 21 as shown below:*

~~The object is achieved by the invention.~~

*On page 2, after line 21, please insert the following heading and paragraphs:*

#### BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1 illustrates a thermostable sample holder useful for assessing emulsion stability.

Figure 2 illustrates the use of a flat bed scanner with the sample holder of Figure 1, and a gray scale plot obtained therefrom.

Figures 3 and 4 depict plots of scattered light intensity as a function of cell height for an unstable emulsion.

Figures 5 and 5a illustrate one method of measuring the contact angle of a partly hydrophoticized filler against water.

Figure 6 illustrates a Zisman plot for determining surface energy.

*On page 2, before line 23, please insert the following heading:*

#### DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

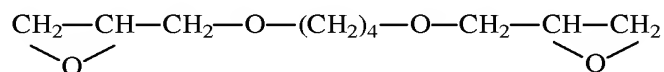
*Please amend the paragraph beginning on page 4, line 34 as shown below:*

Here, non-particulate emulsifiers means not particles and colloids but molecules and polymers, following the definition of molecules, polymers, colloids and particles as given in "Dispersionen und Emulsionen [Dispersions and emulsions]", G. Lagaly, O. Schulz, R. Zindel, Steinkopff, Darmstadt 1997, ISBN 3-7985-1087-3, page 14. In general, these organic emulsifiers have a size of less than 1 nm, a molar mass of  $< \text{~~10,000~~ } \underline{10,000}$  g/mol, a carbon content of  $> 50\%$  by weight, determinable by elemental analysis, and a Mohs' hardness of less than 1.

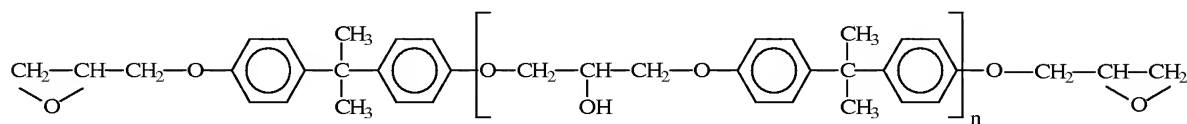
*Please amend the paragraph beginning on page 5, line 27 as shown below:*

The emulsion according to the invention contains an oil phase (phase A). Phase A contains one substantially water-insoluble component, optionally a plurality of substantially water-insoluble components. Here, substantially water-insoluble means that the solubility of the components in water alone or as a mixture is less than 10 g/100 g of water, preferably less than 1 g/100 g of water, particularly preferably less than 0.1 g/100 g of water, measured at 20°C and the pressure of the ambient atmosphere, i.e. from 900 to 1100 hPa. In the case of the emulsion according to the invention, the viscosity of phase A, measured at 20°C and a shear gradient of  $10 \text{ s}^{-1}$ , is from 0.1 to  $\text{~~1,000,000~~ } \underline{1,000,000}$  mPa·s, preferably from 0.1 to  $\text{~~500,000~~ } \underline{500,000}$  mPa·s, particularly preferably from 0.2 to  $\text{~~100,000~~ } \underline{100,000}$  mPa·s. In the case of the emulsion according to the invention, the phase A can preferably contain a plurality of components. The individual components may be both substances which are liquid at 20°C and solids, the total mixture of the individual components having the abovementioned viscosity. Preferably, but not necessarily, a multicomponent phase A is a true solution, i.e. a homogeneous phase in which no further phase interfaces occur.

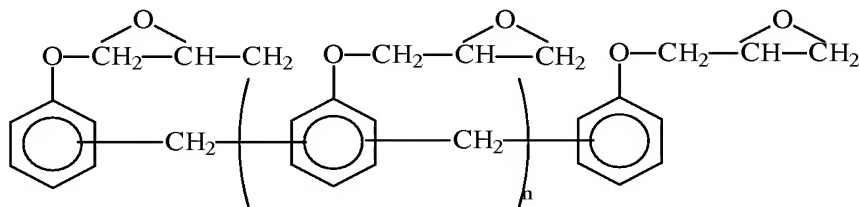
Examples of substantially water-insoluble components as may be formed by the phase A of an emulsion according to the invention or may be present in it are aliphatic and aromatic hydrocarbons, alcohols, aldehydes, ketones, ethers, esters, amines, carboxylic acids and derivatives thereof, mercaptans, thioethers, oligomeric or polymeric compounds, such as polyolefins, such as polystyrenes, polypropylenes or polyethylenes, saturated or unsaturated polyesters, such as, for example, polycondensates of phthalic acids and 1,2-propanediols or polycocondensates of phthalic acids, 1,2-propanediols and maleic acids, optionally dissolved in reactive diluents, such as styrenes, polyethers, polyepoxides or monomeric or oligomeric precursors thereof, such as alkylene bisglycidyl ethers, such as



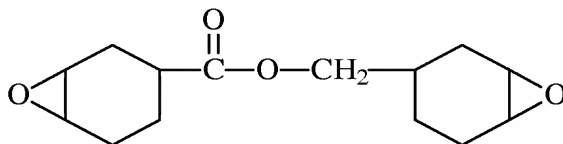
bisphenol A-based diglycidyl ethers, such as



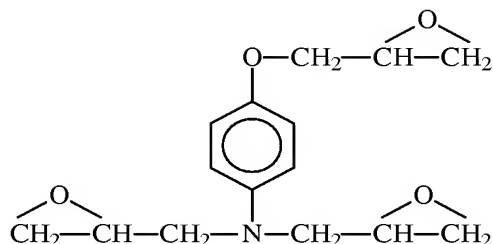
with n preferably from 0 to 10, ~~particularly~~ more preferably from 0 to 5, epoxy novolac resins, such as those of the formula



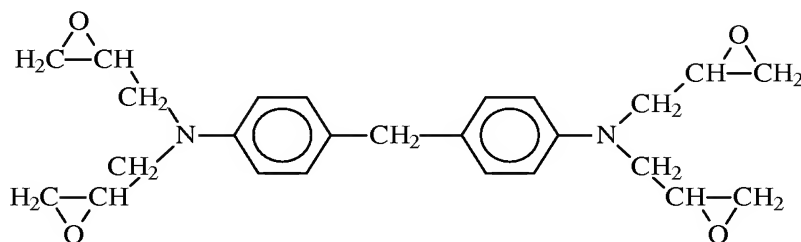
bifunctional epoxy compounds, such as



trifunctional epoxy compounds, such as



tetrafunctional epoxy compounds, such as



polyurethanes or monomeric or oligomeric precursors thereof, such as, for example, polyetherpolyols, polyacrylatepolyols, polyesterpolyols, polyfunctional isocyanates, such as hexane diisocyanate, toluene diisocyanate, diphenylmethane diisocyanate or isocyanates provided with blocking protective groups, such as hydroxylamines or malonic ester derivatives, complex organic compounds, such as synthetic or natural pharmaceutical or cosmetic active substances, dyes, organo-element compounds, such as organosilicon compounds, such as organo(poly)silanes, organo(poly)siloxanes, organo(poly)silazanes and organo(poly)silcarbanes, or transition metal compounds. Optionally, phase A may contain oil-wettable particles, such as pigments, fillers or rheological additives.

*Please amend the paragraph beginning on page 9, line 17 as shown below:*

The sinter aggregates used according to the invention preferably have a solubility in water, at pH 7.33 and an electrolyte background of 0.11 mol and a temperature of 37°C, of less than 0.1

g/l, ~~particularly~~ more preferably [[of]] less than 0.05 g/l, at the pressure of the ambient atmosphere, i.e. between 900 and 1100 hPa.

*Please amend the paragraph beginning on page 9, line 24 as shown below:*

Preferably, the sinter aggregates used according to the invention have a mean hydrodynamic equivalent diameter  $D_h$  of greater than 1 nm, preferably from 1 to 5000 nm, more preferably from 10 to 1000 nm, ~~particularly~~ yet more preferably from 100 to 600 nm, ~~very particularly~~ and most preferably from 200 nm to 500 nm, especially ~~selected~~ from 210 nm to 450 nm, measured in each case preferably by means of dynamic light scattering.

*Please amend the paragraph beginning on page 9, line 33 as shown below:*

This means that the collision radius  $R_c$  of the sinter aggregates which is relevant for the formation of a particle layer in the oil-water interface is greater than 0.8 nm, more preferably from 0.8 to 4000 nm, preferably from 8 to 850 nm, ~~particularly~~ yet more preferably from 80 to 500 nm, ~~very particularly~~ and most preferably from 170 nm to 375 nm. The collision radius is the radius of the smallest sphere which just includes all constituents of an aggregate, the collision radius  $R_c$  being obtained from the equation  $R_c = [R_h^2/0.76 + 2.63 \cdot R_h^2/df]^{0.5}$ , as stated in R. de Rooij, A. A. Potanin, D. van den Ende, J. Mellema, J. Chem. Phys. 1993, 99, 9213, the hydrodynamic equivalent radius  $R_h$  being obtained from the hydrodynamic equivalent diameter divided by 2 and the fractal dimension of the mass  $df$  having a value of 1.8.

*Please amend the paragraph beginning on page 10, line 11 as shown below:*

The sinter aggregates used according to the invention are furthermore preferably characterized in that, in the particle size determination by means of quasielastic light scattering, the hydrodynamic equivalent diameter is at least a factor of 2, preferably a factor of from 5 to 50, ~~particularly~~ more preferably a factor of from 7 to 25, ~~very particularly~~ and most preferably a factor of from 7.5 to 16.5, based in each case on a specific surface area of 100 m<sup>2</sup>/g (the factor decreases or increases in a correspondingly linear manner in the case of a smaller or larger

surface area), greater than the primary particle diameter obtainable computationally according to the formula  $a = 6/A_{\text{BET}} \cdot d$ ,  $A_{\text{BET}}$  being the specific BET surface area measured by means of nitrogen adsorption according to DIN 66131 and  $d$  being the density of the primary particles.

*Please amend the paragraph beginning on page 10, line 30 as shown below:*

The sinter aggregates used according to the invention preferably have a molar mass greater than ~~10 000~~ 10,000 g/mol, ~~particularly more~~ preferably a molar mass of from ~~50 000 to 50 000 000~~ 50,000 to 50,000,000 g/mol, ~~in particular and most preferably~~ from ~~100 000 to 10 000 000~~ 100,000 to 10,000,000 g/mol, measured in each case preferably by means of static light scattering.

*Please amend the paragraph beginning on page 10, line 37 as shown below:*

The sinter aggregates used according to the invention preferably have a specific BET surface area of from 30 to 500 m<sup>2</sup>/g, ~~particularly more~~ preferably from 80 to 300 m<sup>2</sup>/g. The BET surface area is measured by known methods, preferably according to German Industrial Standard DIN 66131 and DIN 66132.

*Please amend the paragraph beginning on page 11 line 6 as shown below:*

The sinter aggregates used according to the invention preferably have a carbon content of less than 50 percent by weight, a Mohs' hardness greater than 1, more preferably greater than 4, and a surface energy gamma of from 30 to 72.5 mJ/m<sup>2</sup> at a temperature of 25°C and the pressure of the ambient atmosphere, i.e. between 900 and 1100 hPa.

*Please amend the paragraph beginning on page 11, at line 10 as shown below:*

~~The sinter aggregates used according to the invention preferably have a Mohs' hardness greater than 1, particularly preferably greater than 4.~~

*Please amend the paragraph beginning on page 11, at line 14 as shown below:*

~~The sinter aggregates preferably have a surface energy gamma of from 30 to 72.5 mJ/m<sup>2</sup> at a temperature of 25°C and the pressure of the ambient atmosphere, i.e. between 900 and 1100 hPa.~~

*Please amend the paragraph beginning on page 11, at line 19 as shown below:*

The silica sinter aggregates used according to the invention preferably have a dispersion fraction of the surface energy gamma-s-D of from 30 to 80 mJ/m<sup>2</sup>, more preferably from 35 to 70 mJ/m<sup>2</sup>, particularly most preferably from 40 to 70 mJ/m<sup>2</sup>, at a temperature of 25°C and the pressure of the ambient atmosphere, i.e. between 900 and 1100 hPa. The dispersion fraction of the surface energy gamma-s-D is measured, for example, according to "Inverse Gas Chromatography" - "Characterisation of Polymers and other Materials", 391 ACS Symposium Series, D R Lloyd, Th C Ward, H P Schreiber, Chapter 18, pages 248-261, ACS, Washington DC, 1989, ISBN 0-8412-1610-X.

*Please amend the paragraph beginning on page 12, at line 16 as shown below:*

Preferably, partly hydrophobized, ~~particularly~~ more preferably partly silylated, silica sinter aggregates are used as silica sinter aggregates for the preparation of the emulsions according to the invention. Here, partly silylated means that neither is the total silica surface unsilylated nor is the total silica surface silylated.

*Please amend the paragraph beginning on page 12, at line 22 as shown below:*

~~Here, partly silylated means that neither is the total silica surface unsilylated nor is the total silica surface silylated.~~



*Please amend the paragraph beginning on page 12, at line 26 as shown below:*

The degree of coverage  $\tau$  of the surface of the silica sinter aggregates with silylating agent radicals is preferably from 5 to 95%, ~~particularly~~ more preferably from 10 to 90%, in particular from 15% to 75%, based on the total particle surface.

*Please amend the paragraph beginning on page 13, at line 1 as shown below:*

Partial silylation furthermore means that the content of non-silylated surface silanol groups on the silica surface is from not more than 95% to not less than 5%, ~~particularly~~ more preferably from 90 to 10%, in particular from 85 to 25%, of the silanol groups of the starting silica.

*Please amend the paragraph beginning on page 13, at line 8, as shown below:*

This means that the density of the surface silanol groups SiOH is preferably from not less than 0.1 to not more than 1.7, preferably from 0.2 to 1.6, ~~particularly~~ more preferably from 0.45 to 1.55, SiOH per nm<sup>2</sup> of particle surface.

*Please amend the paragraph beginning on page 13, at line 14 as shown below:*

For a starting silica of 200 m<sup>2</sup>/g of specific surface area, which can be used for the silylation, this preferably means not less than 0.03 mmol/g of SiOH and not more than 0.57 mmol/g of SiOH, preferably from 0.06 to 0.54 mmol/g of SiOH, ~~particularly~~ more preferably from 0.15 to 0.51 mmol/g of SiOH; for a silica having a smaller or large surface area, this means linearly proportionally more or less surface silanol groups SiOH.

*Please amend the paragraph beginning on page 13, at line 24 as shown below:*

The silicas used according to the invention have a carbon content of from 0.1 to 20% by weight, preferably from 0.1 to 15% by weight, ~~particularly~~ more preferably from 0.1 to 10% by weight.

*Please amend the paragraph beginning on page 14, at line 4 as shown below:*

The starting silica preferably has a fractal dimension of the surface of preferably less than or equal to 2.3, the fractal dimension of the surface  $D_s$  being defined here as: particle surface A is proportional to the particle radius R to the power of  $D_s$ . Preferably, the starting silica has a density of accessible surface silanol groups SiOH, i.e. accessible to a chemical reaction, of preferably from 1.5 to 2.5 SiOH per  $\text{nm}^2$  of specific surface area, ~~particularly~~ more preferably from 1.6 to 2.0 SiOH per  $\text{nm}^2$ .

*Please amend the paragraph beginning on page 17, at line 25 as shown below:*

Further examples of organosiloxanes are silicone resins, in particular those which contain methyl groups as alkyl groups, ~~particularly~~ more preferably those which contain  $\text{R}^3\text{SiO}_{1/2}$  and  $\text{SiO}_{4/2}$  units or those which contain  $\text{R}^3\text{SiO}_{3/2}$  and optionally  $\text{R}^3_2\text{SiO}_{2/2}$  units,  $\text{R}^3$  having one of the abovementioned meanings.

*Please amend the paragraph beginning on page 20, at line 19 as shown below:*

Alternatively, acidic or basic catalysts can preferably be added. These catalysts may have a basic character in the sense of a Lewis base or a Brønsted base, such as ammonia, or acidic character, in the sense of a Lewis acid or a Brønsted acid, such as hydrogen chloride. If catalysts are used, traces are preferred, i.e. less than 1000 ppm. ~~Particularly~~ Most preferably, no catalysts are added.

*Please amend the paragraph beginning on page 21, at line 31 as shown below:*

In the case of the emulsions according to the invention, the volume fraction  $\Phi_o$  of the oil phase, defined as  $\Phi_o = \text{volume of oil phase} / (\text{volume of oil phase} + \text{volume of water phase})$ , can preferably be from 0.1 to 0.9, preferably from 0.2 to 0.8, ~~particularly~~ more preferably from 0.3 to 0.7, and in particular from 0.4 to 0.6.

*Please amend the paragraph beginning on page 22, at line 1 as shown below:*

In the case of the emulsions according to the invention, the volume fraction  $\Phi_w$  of the water phase, defined as  $\Phi_w = \text{volume of water phase} / (\text{volume of oil phase} + \text{volume of water phase})$ , can preferably be from 0.1 to 0.9, preferably from 0.2 to 0.8, ~~particularly~~ more preferably from 0.3 to 0.7, and in particular from 0.4 to 0.6.

*Please amend the paragraph beginning on page 22, at line 9 as shown below:*

The emulsions according to the invention are characterized in particular in that the mean particle size of the disperse phase, i.e. the mean drop diameter, measured by means of laser diffraction, for example on a laser diffraction apparatus from Sympatec by the cell measuring technique, is preferably from 0.5  $\mu\text{m}$  to 500  $\mu\text{m}$ , more preferably from 0.7  $\mu\text{m}$  to 100  $\mu\text{m}$ , ~~particularly~~ still more preferably from 0.7  $\mu\text{m}$  to 50  $\mu\text{m}$  and ~~very particularly~~ most preferably from 0.7  $\mu\text{m}$  to 10  $\mu\text{m}$ .

*Please amend the paragraph beginning on page 22, at line 19 as shown below:*

The sinter aggregate-stabilized emulsions according to the invention are characterized in particular in that they have a low viscosity. Here, low viscosity means that the emulsions according to the invention have relative viscosities  $\eta_r$  in the range of from 1 to  $10^6$ , preferably from 1 to  $5 \cdot 10^5$ , ~~particularly~~ more preferably less than  $10^5$ . The relative viscosity is defined as the quotient  $\eta_{\text{rel}} = \eta / \eta_0$  of the measured viscosity of emulsion  $\eta$ , measured at 25°C using a cone-and-plate system with a measuring gap of 10<sup>5</sup>  $\mu\text{m}$  and a shear rate  $D = 10 \text{ s}^{-1}$ , divided by the viscosity of the pure homogeneous phase  $\eta_0$ , measured at 25°C.

*Please amend the paragraph beginning on page 23, at line 3 as shown below:*

The particle-stabilized emulsions according to the invention are distinguished in particular by the fact that they are substantially stable to separation of the disperse phase, i.e. substantially stable to creaming or sedimentation of the disperse phase. Here, substantially stable to

separation means that the volume of the phase depleted in dispersion is less than 10% of the total volume, preferably less than 5% of the total volume, ~~particularly~~ more preferably less than 1% of the total volume.

*Please amend the paragraph beginning on page 23, at line 31 as shown below:*

~~See figure 1. Thermostatable sample holder~~

*Please amend the paragraph beginning on page 23, at line 37 as shown below:*

~~See figure 2: Design of the stability analyzer~~

*Please amend the paragraph beginning on page 24, at line 1 as shown below:*

Each sample holder contains up to 12 samples, and all together 24 samples per measuring process can be investigated simultaneously. Image generation will be effected by a procedure in which the light of the scanner lamp is deflected laterally onto the measuring cells by a tilted mirror. At the same time, the emulsion is transilluminated through the bottom of the cell (thick ~~arrow~~ arrows in fig. 2). The scattered light produced by the emulsion (dashed arrows in fig. 2) is then deflected back by the mirror to the sensor of the flat-bed scanner. The light path can be adjusted by adjusting screws (not shown for the sake of clarity). For protecting the scanner from contamination and the samples from heat due to the scanner lamp, a 2 mm thick plexiglass screen is also present on the scanner window.

*Please amend the paragraph beginning on page 24, at line 35 as shown below:*

Evaluation is now effected by plotting the measured scattered light intensity as a function of the height measured from the bottom of the cell. Measurements at defined distances are carried for evaluating the stability of an emulsion. A plot of  $\Delta I(z,t) = I(z,t) - I(z,0)$ , where  $I(z,t)$  is the scattered light intensity at the height  $z$  at time  $t$  and  $I(z,0)$  is the scattered light intensity at the height  $z$  at the time 0, gives the change in the scattered light intensity with time. A positive

change means a higher concentration of scattering particles and therefore indicates separation of the emulsion; analogously, a decrease in the scattered light intensity in a certain volume element as a function of time is a depletion of particles capable of scattering in this element. Figures 3 and 4 illustrate this by way of example for an unstable emulsion.

*Please amend the paragraph beginning on page 25, at line 14 as shown below:*

~~Figures 3 and 4 illustrate this by way of example for an unstable emulsion.~~

*Please amend the paragraph beginning on page 26, at line 32 as shown below:*

The concentration of the silica sinter aggregates in the dispersion is between 1 and 80% by weight, preferably between 10 and 60% by weight, ~~particularly~~ more preferably between 10 and 40% by weight and ~~very particularly~~ most preferably between 12 and 30% by weight.

*Please amend the paragraph beginning on page 28, at line 4 as shown below:*

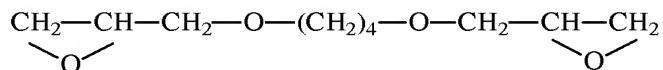
The temperature of the liquid phase during the emulsification process is between 0°C and 80°C, preferably between 10°C and 50°C, ~~particularly~~ more preferably between 20°C and 40°C.

*Please amend the paragraph beginning on page 28, at line 9 as shown below:*

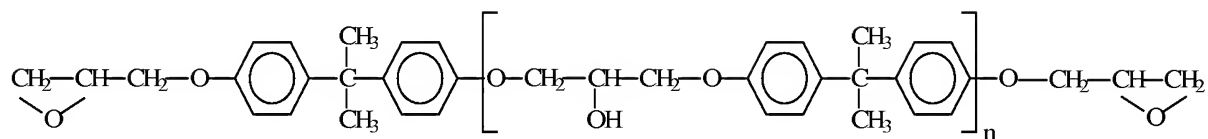
The emulsification process can be carried out at atmospheric pressure, i.e. at from 900 to 1100 hPa, at elevated pressure, or in vacuo. The process at atmospheric pressure is preferred.

*Please amend the paragraph beginning on page 29, at line 31 as shown below:*

Examples of epoxy compounds are alkylene bisglycidyl ethers, such as



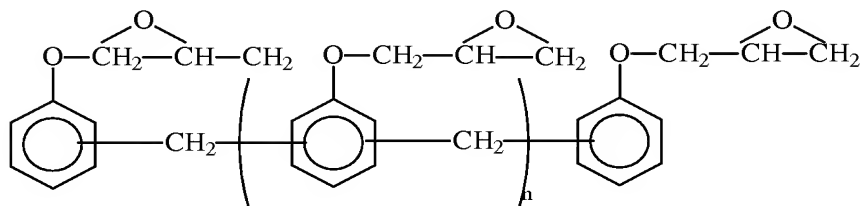
bisphenol A-based diglycidyl ethers, such as



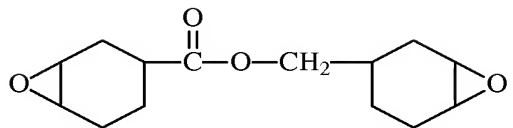
with n preferably from 0 to 10, particularly preferably from 0 to 5.

*Please amend the paragraph beginning on page 30, at line 8 as shown below:*

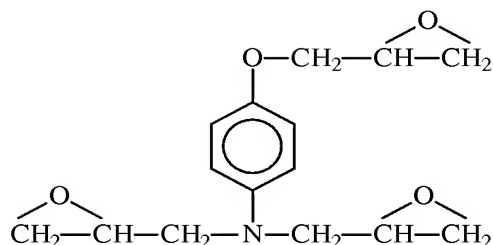
Examples of epoxy novolac resins, ~~such as~~ are those of the formula



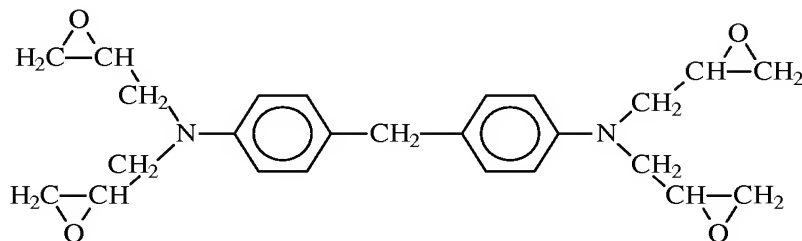
bifunctional epoxy compounds, such as



and trifunctional epoxy compounds, such as



tetrafunctional epoxy compounds, such as



*Please amend the Table beginning on page 33, at line 1 as shown below:*

Property	Silica B1 according to Example 1
BET surface area	184 m <sup>2</sup> /g
Residual content of non-silylated silica silanol groups	80%
Carbon content %C	0.5% by weight
Methanol number	0
Contact angle THETA Method 1 against water and air	84°
Contact angle THETA Method 2 against water and air	of 80°
Surface energy GAMMA	69 MJ/m <sup>2</sup>
Dispersion fraction of surface energy GAMMA-s-D	65 mJ/m <sup>2</sup>

*Please amend the paragraph beginning on page 34, at line 31 as shown below:*

Contact angle THETA method 2 against water, measured as by means of an imbibition method using the ~~Lukas~~ Lucas-Washburn equation, based on the aspiration of a known and defined liquid, with a known surface tension, into a defined ~~heap~~ specimen, in this case a slightly compacted pellet of the silica having an open porosity greater than 0.25 and a pore radius  $r$ . The aspiration rate  $dh/dt$  and the height of the aspirated liquid column  $h$  are calculated from the mass absorption  $m$  of liquid by the particle heap as a function of the time  $t$ , and the viscosity of the aspirated liquid  $\eta$  and the surface tension  $\gamma$  of the aspirated liquid make it possible, in the case of a known particle radius  $r$ , to calculate the cosine value of  $\theta$  ( $\cos(\theta)$ ) and hence the contact angle  $\theta$  of the liquid against the particle surface by means of the equation according to Lucas-Washburn (Washburn, E.W., Phys. Rev. 17, 273 (1921) and R. Lucas, Kolloid s. 23, 15 (1918)); following J. Schoelkopf et al., J. Colloid. Interf. Sci. 227, 119-131 (2000).

*Please replace Table 2 beginning on page 38, at line 8 as shown below:*

Property	<del>Aqueous Dispersion from</del> Example 1
<del>Solids content</del>	16.1%
pH	5.3
<del>Mean diameter</del>	302 nm
<del>Sinter aggregates</del>	
<del>Viscosity</del>	240 mPas



Property	Aqueous Dispersion from Example 1
Solids content	16.1 %
pH	5.3
Mean diameter Sinter aggregates	302 nm
Viscosity	240 mPas

*Please amend the paragraph beginning on page 38, at line 10 as shown below:*

- Solids content of the dispersion determined by the following method: 10 g of aqueous dispersion are mixed with the same amount of ethanol in a porcelain dish and evaporated to constant weight in an N<sub>2</sub>-flushed drying oven at 150°C. The mass  $m_s$  of the dry residue gives the solids content according to  $\text{solids content}/\% = m_s \cdot 100/10 \text{ g}$ .
- pH measured by means of a pH combination electrode
- mean diameter of the sinter aggregates measured by means of photocalorrelation spectroscopy by the following method: 4 samples of the dispersion to be measured which have a silica content of 1 % by weight, 0.75 % by weight, 0.5 % by weight and 0.25 % by weight are prepared in demineralized water by stirring in the appropriate amount of starting dispersion by means of a magnetic stirrer. The samples are measured in a PCS apparatus Coulter N4 Plus from Coulter at detection angles of 30.1°, 62.6° and 90°. The mean diameter of the sinter aggregates is obtained by extrapolating the angle-dependent measured values obtained to a silica content of 0 % by weight and then averaging over the three measured angles.

*Please amend the paragraph beginning on page 39, at line 8 as shown below:*

78 g of the above-described silica dispersion having a solids content of 16% by weight are initially introduced into a 500 ml stainless steel beaker. 150 g of a polydimethylsiloxane having

a viscosity of 100 mPas (obtainable under the name "AK100" from Wacker-Chemie GmbH, Munich, Germany) are slowly metered in over a period of 15 min with stirring at ~~10-000~~ 10,000 rpm using an Ultraturrax and while cooling with water. The temperature of the mixture should not exceed 60°C. 86 g of demineralized water are then slowly added over a period of 15 min, likewise at ~~10-000~~ 10,000 rpm, to this now highly viscous stable material. The temperature of the mixture should not exceed 60°C. A low-viscosity white O/W emulsion results, the analytical data of which are summarized in Table 3.

*Please amend the paragraph beginning on page 39, at line 26 as shown below:*

78 g of silica dispersion according to Example 1 are initially introduced into a 500 ml stainless steel beaker. While stirring at ~~10-000~~ 10,000 rpm using an Ultraturrax and while cooling with water, 150 g of methyl nonanoate are metered in slowly over a period of 15 min. The temperature of the mixture should not exceed 60°C. 86 g of demineralized water are then slowly added over a period of 15 min, likewise at ~~10-000~~ 10,000 rpm, to this now highly viscous stable material. The temperature of the mixture should not exceed 60°C. A low-viscosity white O/W emulsion results, the analytical data of which are summarized in Table 3.

*Please amend the paragraph beginning on page 40, at line 3 as shown below:*

150 g of an OH-terminated polydimethylsiloxane having a viscosity of 1000 mPas (obtainable under the name "OH 1000" from Wacker-Chemie GmbH, Munich, Germany) are initially introduced into a 500 ml stainless steel beaker. While stirring at ~~10-000~~ 10,000 rpm using an Ultraturrax and while cooling with water, 78 g of silica dispersion according to Example 1 are slowly metered in over a period of 15 min. The temperature of the mixture should not exceed 60°C. 86 g of demineralized water are then slowly added over a period of 15 min, likewise at ~~10-000~~ 10,000 rpm, to this now highly viscous stable material. The temperature of the mixture should not exceed 60°C. A low-viscosity white O/W emulsion results, the analytical data of which are summarized in Table 3.

*Please amend the paragraph beginning on page 40, at line 21 as shown below:*

78 g of silica dispersion according to Example 1 are initially introduced into a 500 ml stainless steel beaker. While stirring at ~~10-000~~ 10,000 rpm using an Ultraturrax and while cooling with water, 150 g of a solution of 125 g of the epoxy resin Epikote 828 in 25 g of xylene are metered in slowly over a period of 15 min. The temperature of the mixture should not exceed 60°C. 86 g of demineralized water are then slowly added over a period of 15 min, likewise at ~~10-000~~ 10,000 rpm, to this now highly viscous stable material. The temperature of the mixture should not exceed 60°C. A low-viscosity white O/W emulsion results, the analytical data of which are summarized in Table 3.

*Please amend the paragraph beginning on page 40, at line 37 as shown below:*

5 g of partly hydrophobic silica having a degree of hydrophobing of 50% and a carbon content of 1.1% (obtainable under the name "Wacker HDK H20" from Wacker-Chemie GmbH, Munich, Germany) are stirred into 85 g of isododecane in a 500 ml stainless steel beaker by means of a dissolver having a toothed disk, and dispersing is then effected for 10 min at ~~10-000~~ 10,000 rpm. 120 g of demineralized water are slowly metered over a period of 15 min into this now highly viscous dispersion with stirring at ~~10-000~~ 10,000 rpm using an Ultraturrax and while cooling with water. The temperature of the mixture should not exceed 60°C. 95 g of isododecane are then slowly added over a period of 15 min to the resulting stable material at 1000 rpm. The temperature of the mixture should not exceed 60°C. A low-viscosity white W/O emulsion results, the analytical data of which are summarized in Table 3.

*Please amend the paragraph beginning on page 41, at line 18 as shown below:*

94 g of the silica dispersion from Example 1, having a solids content of 16% by weight, are initially introduced into a 500 ml stainless steel beaker. 180 g of a polydimethylsiloxane having a viscosity of 100 mPas (obtainable under the name "AK100" from Wacker-Chemie GmbH, Munich, Germany) are slowly metered in over a period of 15 min with stirring at ~~10-000~~ 10,000 rpm using an Ultraturrax and while cooling with water. The temperature of the mixture

should not exceed 60°C. 41 g of demineralized water are then slowly added over a period of 15 min, likewise at ~~10-000~~ 10,000 rpm, to this now highly viscous stable material. The temperature of the mixture should not exceed 60°C. A low-viscosity white O/W emulsion results, the analytical data of which are summarized in Table 3.